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# **THE CALCULATION OF MULTICOMPONENT MIXTURE PHASE DIAGRAM, USING THE EQUATIONS OF STATE OF THE VAN DER WAALS TYPE**

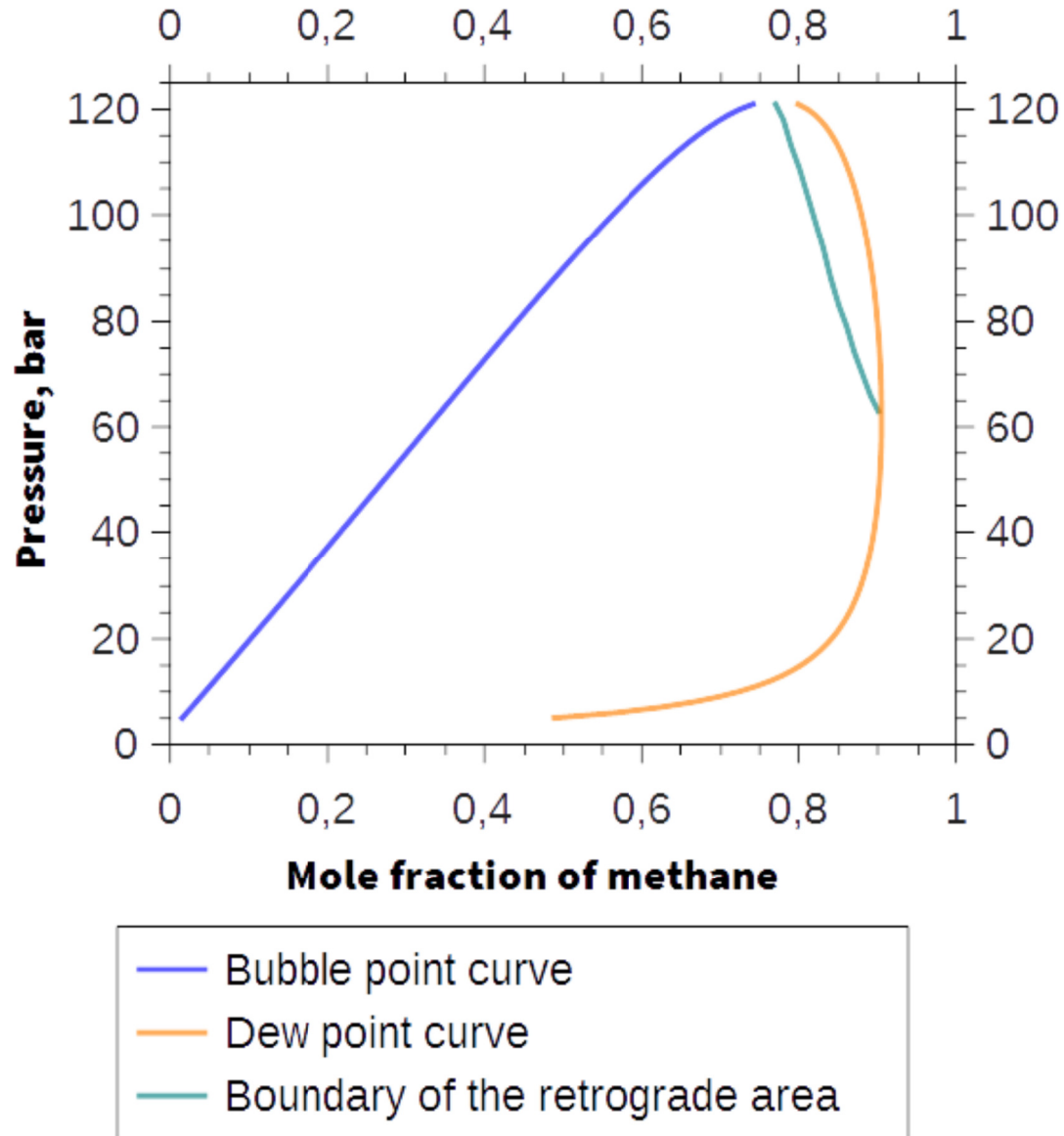
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# Phase diagram of a gas-condensate mixture

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Phase diagram of methane-n-butane mixture at 293 K

# Equation of state

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$$p + \frac{a}{(v+c)(v+d)} = \frac{RT}{(v-b)},$$

Where:  $p$  — pressure,  $T$  — temperature,  $R$  — gas constant,  $V$  — mole volume,  
 $a$ ,  $b$ ,  $c$ ,  $d$  — coefficients of the equation of state

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$$a = a_c \varphi(T),$$

$$a_c = \alpha \frac{R^2 T_c^2}{P_c},$$

$$\varphi(T) = \left( 1 + \psi \left( 1 - \left( \frac{T}{T_c} \right)^{0.5} \right) \right)^2,$$

$$b = \beta \frac{RT_c}{P_c},$$

$$c = \sigma \frac{RT_c}{P_c},$$

$$d = \delta \frac{RT_c}{P_c}.$$

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$$\alpha = \Omega_c^3,$$

$$\beta = Z'_c + \Omega_c - 1,$$

$$\delta = -Z'_c + \Omega_c \left( 0.5 - (\Omega_c - 0.75)^{1/2} \right).$$

$$\sigma = -Z'_c + \Omega_c \left( 0.5 + (\Omega_c - 0.75)^{1/2} \right)$$

# Algorithm

## System of the equations

$$f_{Li} - f_{Vi} = 0$$

$$x_i L + y_i V - \eta_i = 0$$

$$\sum_{i=1}^N y_i - 1 = 0$$

$$L + V = 0$$

## Initial data for the mixture:

- Composition,
- Pair coefficients,
- P — pressure,
- T — temperature,

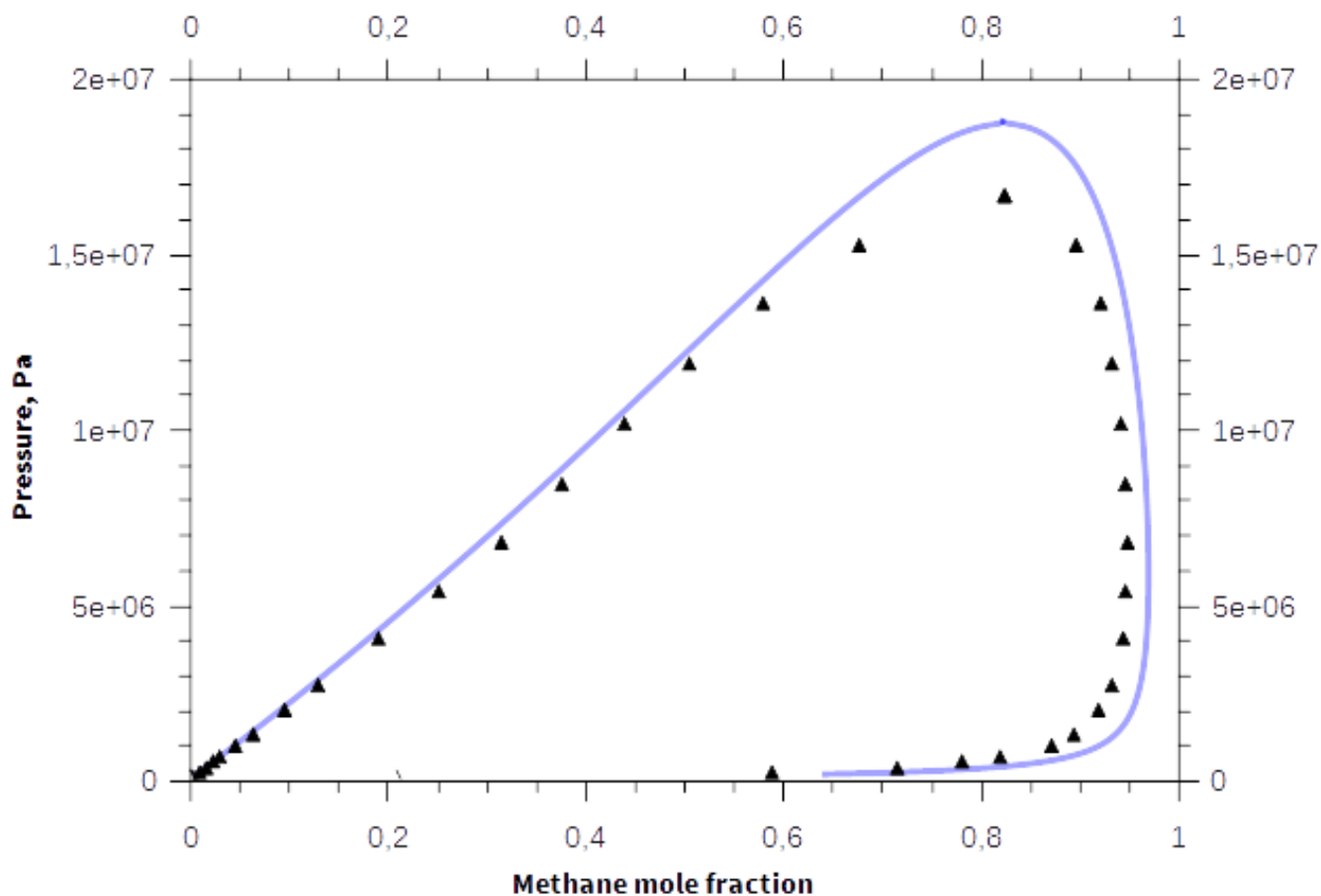
## Initial data for components:

- $P_c$  — critical pressure,
- $T_c$  — critical temperature,
- $\omega$  — acentric factor,
- $\Omega_c, Z'_c, \psi$  — parameters of the equation of state

Component	$\Omega_c$	$Z'_c$	$\psi$
$N_2$	0.75001	0.34626	0.37182
$CO_2$	0.75282	0.31933	0.74212
$H_2S$	0.78524	0.30418	0.38203
$CH_4$	0.7563	0.33294	0.37447
$C_2H_6$	0.77698	0.31274	0.4955
$C_3H_8$	0.76974	0.31508	0.53248
i- $C_4H_{10}$	0.78017	0.30663	0.63875
n- $C_4H_{10}$	0.76921	0.31232	0.57594

# Calculated phase diagrams

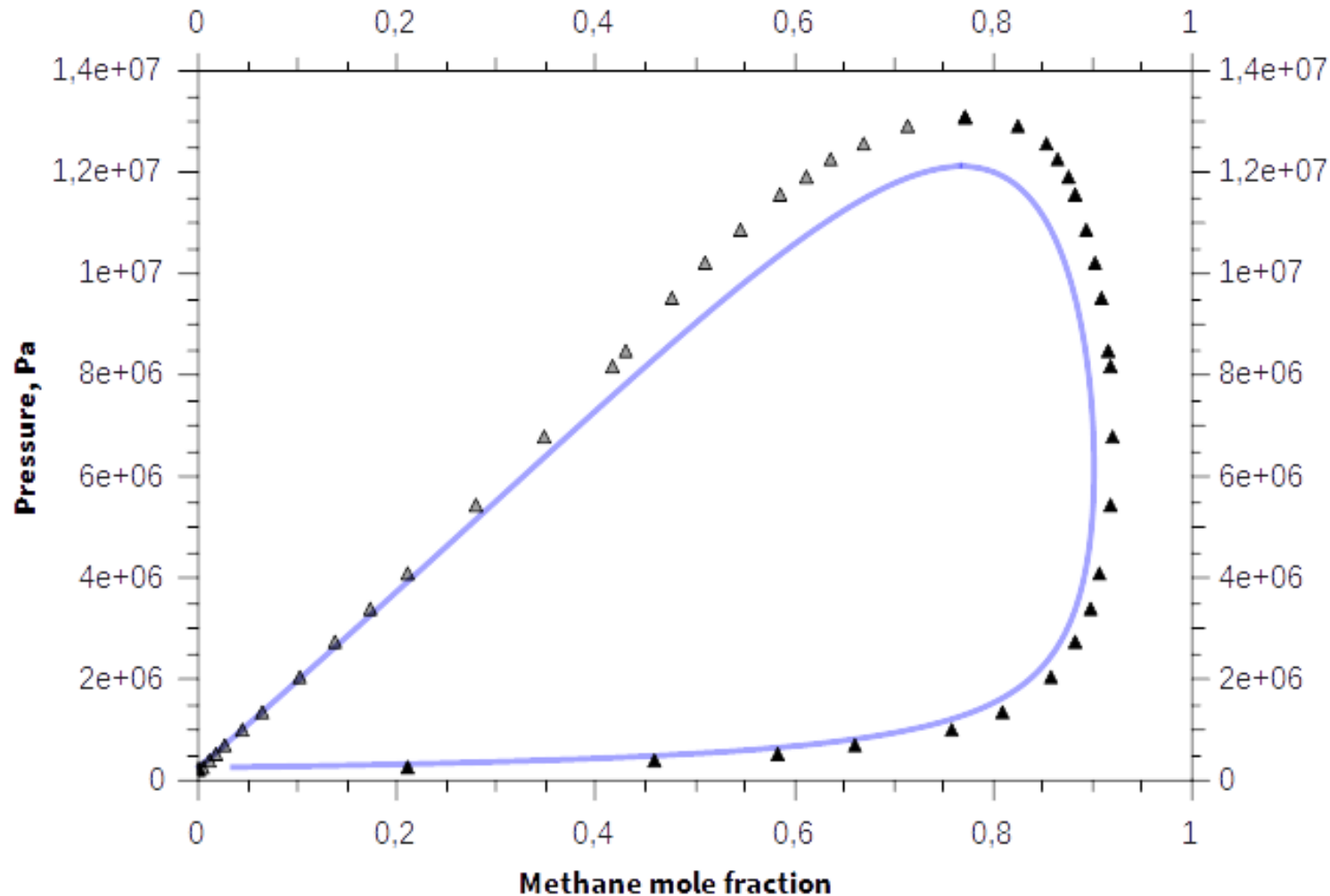
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## Phase diagramm of the methane-n-pentane mixture at 311 K

Blue line — calculation, black points — experimental data by Kogan V.B., Fridman V.M., Kafarov V.V. Liquid-vapour equilibrium. Volume 1 // M.: "Nauka", 1966, 646 p.

# Calculated phase diagrams



## Phase diagramm of the methane-n-butane mixture at 294 K

Blue line — calculation, black points — experimental data by Kogan V.B., Fridman V.M., Kafarov V.V. Liquid-vapour equilibrium. Volume 1 // M.: "Nauka", 1966, 646 p.

# Conclusions

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- **Software package to calculate the vapor-liquid equilibrium of multicomponent systems has been created.**
- **The possibility to calculate phase equilibrium via cubic equation of state of the Van der Waals type is shown.**

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Thank you for your attention!

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